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Chemical Modification of Activated Carbon and Its Application for Solid Phase Extraction of Copper(II) and Iron(III) Ions

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Powder activated carbon surface (AC) was modified and altered procedure thorough a facile and easy chemical reaction to appearance of 2-((3-silylpropylimino)-1-methyl) phenol (AC-(SPIMP)). Subsequently, this novel sorbent efficiently applied for the extraction and preconcentration of some metal ions from real samples. Preliminary the influences of variables such as pH, amounts of reagents and porous AC, eluting solution conditions (type and concentrations), sample volume and influence of interference of many ions on the analytes recoveries was studied and optimized. The proposed sorbent has high surface area (>1317.1346 m² g⁻¹) and small pore size (<37.750 A). The acceptable relative standard deviations (n = 10, <4.5%) and detection limit based on $3S_b/m$ (*n* = 10) was 1.2-2.6 ng ml⁻¹ and their preconcentration factor was 100 with large adsorption capacity (45.3 mg g⁻¹). The proposed method was successfully applied for the extraction and determination of analytes in different samples.

Keywords: Chemical modification, Activated carbon, Solid phase extraction, Pore size distribution, BET analysis

INTRODUCTION

The monitoring of trace metals level with double role (vital and toxic nature) is a important task. In this regard concern to analytical chemists and research focus on the environmental and pollution studies [1-5]. One of the difficult task of analytical chemistry is the main limitations encountered for the quantification of metal ions by flame atomic absorption spectrometry (FAAS) at trace levels in complicated matrices [6-14]. This purpose, simply achieved by combination of preliminary separation and/or enrichment stages before detection that permit accurate, reliable and sensitive results even at analyte too low concentration [15-29]. Appropriate selection of supports and their subsequent modification by physical or chemical pathways is a great demand. These modifications by different shape, functional group and structure significantly influence the ability and tendency of modified support toward separation and/or concentration of target compounds. Versatile separation

procedures are recommended for selective and efficient concentration and/or separation of analytes from complicated sample matrices. Amongst, solid phase extraction (SPE) come to the forefront compared to other separation/enrichment methods because of their unique associated advantages [30-33]. Sorption and chelate extraction is frequently applicable techniques for metal ions recoveries from low-concentration solutions.

One of the most general and traditionally know support is activated carbon that has highly porous structure with various functional group. This reagent is for binding different targets by hydrogen bonding, π -donating-accepting and hydrogen bonding and at some pH *via* electrostatic interaction. The analytes adsorption on such sorbent strongly affected by the amount of aromatic rings and π - π bonds. Generally, functionalization and/or activation can substantially improve the hydrophilic character of the AC and modify its pore volume and specific surface area [34-37].

The large surface area and surface hydrophobicity in addition to surface oxygen and functional groups, make

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possible the adsorption of different compounds on AC, The adsorption process severely control their adsorption by parameters such as pH [38].

Usage of AC chemically functionalized by various organic compounds good mechanical and thermal stability has lower abbility, to swell and shrink [39]. Selective binding fashion of sorbent depend to factors such as size and funtional and reactive group of of the modifier (hard-soft and/or acid-base concept). Presence of huge number of reactive sites on it surface make possible easy modification therough different mechanism. Impergeation of various chelating agent on AC change the possible mechanism of metal ions retardation through surface complex formation between the metal ions and the acidic non-selective surface functional groups. The other sites fashionably imbedded on the AC surface greatly altered the surface area (adsorption capacity) and pore properties of the AC and finally decrease the adsorption equilibrium time.

The adsorption properties of AC depend to its surface chemical nature, its surface area and porosity and acidic surface functional groups. Modification of the surface chemistry of activated carbons is an attractive route toward novel applications of these materials as adsorbent for heavy metal removal. The presence of acidic functional groups on AC enhances their hard metal ions sorptive capacities, while has low tendency for the adsorption of soft metal ions. The AC surface modifications lead to the change in the surface reactivity, chemical, physical and structural properties. Activated carbons (AC) are widely used as adsorbents because of their high specific surface areas, well-developed tunable porosities, and surface oxygen-containing complexes.

In the present work, a new simple SPE based on chemical functionalization of porous AC was developed and the influence of effective variables for extraction, preconcentration and determination of Cu^{2+} and Fe^{3+} ions in real samples has been optimized. After elution by suitable stripping agent, the concentration of analytes in the eluent was determined by AAS to calculate the desorption yield.

EXPERIMENTAL

Instruments

These understudy metal ions content determination were carried out using Shimadzu 680 AA atomic absorption

spectrometer with a hallow cathode lamp and deuterium background corrector according to respective wavelengths (resonance line) using an air-acetylene flame. pH of the solution was maintained by using 0.1 M HCl and 0.1 M NaOH solutions using a pH/Ion meter model 692 Metrohm.

Reagents

Acids and bases (with the highest purity available from Merck, Darmstadt, Germany) solution was prepared in doubly distilled deionized water. Nitrate salts of cadmium, mercury, copper, magnesium, calcium, strontium, barium, silver, sodium and potassium (all from Merck) were of the highest purity available and used without any further purification. Commercial activated carbon (AC) with the highest purity available are purchased from Merck (Darmstadt, Germany) was used as received without any purification.

Preparation of 2-((3-Silylpropylimino)-1-methyl) phenol Bonded to Porous Activated Carbon (AC-(SPIMP))

In preliminary stage, ACs powder was purified and activated with 10% (v/v) hydrochloric acid solution for 24 h to remove adsorbed impurities and metal ions. Then, it was filtered, washed with distilled deionized water and dried at 80 °C for 5 h. Functionalization of AC was carried out as follow: 1 g of purified AC was suspended in 250 ml of 32.5% (v/v) nitric acid solution under stirring for 36 h at room temperature. Subsequently the mixture was filtered and thoroughly rinsed with distilled deionized water to neutral and dried at 80 °C for 2 h. The Schiff base modified AC was prepared based on following procedure. ACsupported silyl-aminopropyl was synthesized by refluxing 1 g of functionalized AC with 1.8 ml of trimethoxysilylpropylamine (TMSPA) in dichloromethane (20 ml) for 24 h and the solid was filtered and dried at room temperature. Then 0.9 ml of 2-hydroxyacetophenone (2-HAP) was added to a suspension of AC-supported silyl-aminopropyl in methanol (20 ml). Then the reaction mixture was refluxed for 24 h and then filtered, washed with distilled water and dried at room temperature to obtain a greenish black precipitate as a chemically modified AC-2-((3silylpropylimino)-1-methyl) phenol (AC-(SPIMP)) [40]. The schematic diagram of preparation of this new sorbent is presented in Fig. 1.

Column Preparation

A short glass column with an inner diameter of 0.5 cm and a length of 50 cm, equipped with porous frits was filled up to a height of about 1 cm with a suspension of 1 g of (AC-(SPIMP)) and subsequently preconditioned by the blank solution prior to each use and after using the column was rinsed with water and stored for the next experiment.

Preconcentration Procedure

The procedure was examined by using model test solutions. The pH of 250 ml of sample solution containing 0.01-0.5 μ g ml⁻¹ of all analytes was adjusted in the range of 2.0-8.0 by addition of NaOH and/or HCl solution. The solutions were passed through the column containing 1 g present sorbent at flow rate of 4 ml min⁻¹. The retention and uptake of under study metal ions took place following complication with modifier chemically impregnated on the AC surface. The adsorbed ions were then eluted with 6 ml of 4.0 M nitric acid (1 ml min⁻¹) and their content in the eluent were determined by flame atomic absorption spectrometer.

Analysis of the Real Samples

All real samples (banana, tomato and strawberry) were purchased from Yasouj, Iran. A 40 g of all real samples was heated in silica crucible for 3 h on a hot plate and the overcooked material was transferred to furnace for overnight heating at 650 °C. The residue was cooled, treated with 10.0 ml concentrated nitric acid and 3 ml 30% H₂O₂ again kept in furnace for 2 h at the same temperature so that no organic compound traces are left. The final residue was treated with 3 ml concentrated hydrochloric acid and 2-4 ml 70% (w/w) perchloric acid and evaporated to fumes, so that all the metals change to respective ions. The solid residue was dissolved in water, filtered and by keeping the pH at 4.0 made up to 250 ml by addition of KOH and phosphate buffer. The dissolved solution was suitably diluted and metal concentrations were determined by FAAS after application to preconcentration procedure given above.

RESULTS AND DISCUSSION

Characterization of Adsorbent (AC-(SPIMP))

Low temperature N2 adsorption isotherms (Fig. 1) show the type I BET isotherm in the IUPAC classification [41].



Fig. 1. Schematic diagram for the synthesis of the proposed sorbent (AC-(SPIMP)).



Fig. 2. BET plot of adsorbent and its pore size distribution.

According to analysis of these data, the total pore volume, micropore volume and surface area were calculated and their value is listed in Table 1. The high surface area and internal pore of adsorbent allow enriching high amount of metal ions following its chemical modification. On the other

Surface are $(m^2 g^{-1})$					
Single point surface area at $p/p = 0.211926089$	1317.1346				
BET surface Area	1332.2981				
Langmuir Surface Area	1827.0887				
t-Plot Micropore Area	630.9017				
t-Plot External Surface Area	701.3964				
BJH Adsorption cumulative surface area of pores	128.449				
between 17.000 A and 3000.000 A width					
BJH Desorption cumulative surface area of pores	146.9493				
between 17.000 A and 3000.000 A width					
Pore volume (cm ³ g ⁻)					
Single point adsorption total pore volume of pores	0.664918				
less than 1191.414 Å width at $p/p^{\circ} = 0.983478638$					
t-Plot micropore volume	0.278830				
BJH Adsorption cumulative volume of pores	0.121225				
between 17.000 Å and 3000.000 Å width					
BJH Desorption cumulative volume of pores	0.126545				
between 17.000 Å and 3000.000 Å width					
Pore size (Å)1					
Adsorption average pore width (4V/A by BET)	19.9630				
BJH Adsorption average pore width (4V/A)	37.750				
BJH Desorption average pore width (4V/A)	34.446				

Table 1. Surface Properties and Pore Size Distribution of proposed Adsorbent

hand, immobilization of high amount of modifier on its surface is possible that increase the number of reactive atom and surface volume to area ratio.

The SEM investigation of porous AC before and after chemical modification show its homogenous sites with nanometers scale lower than 100 nm (Figs. 3, 4). IR spectra of AC, surface supported aminopropylsilylate and AC-(SPIMP)) are shown in Fig. 5A-B. IR spectrum of AC shows some important characteristic vibrational frequencies at 3400-2500(bw), 1627(w), 1155(s), 673(s), 592(s) that may be assigned to hydroxyl, carbonyl, olefinic groups (Fig. 5-A). After loading of trimethoxysilylpropylamine on AC surface, some additional characteristic absorption bands at 2929(w), 3200-3350(weak fine structure), 1563(m), 1405(w), 1300(w), 1121(s), 1031(s), 678(s), and 594(w) are appeared in IR spectrum of AC-supported aminopropylsilylate that can be related to bending of NH-stretching, NH-bending, NH_2 -scissoring, CH_2 -bending and CH_2 rocking of compound (Fig. 5-B).

Finally 2-hydroxyacetophenone (2-HAP) is bounded to surface supported aminopropylsilylate *via* an iminic bound to obtain a chemically modified AC with 2-((3silylpropylimino)-1-methyl) phenol (AC-(SPIMP)) as extractor. IR spectrum well exhibits some characteristic peaks at 3422(m), 2924(w), 2857(w), 1588(s), 1400-1550(m), 1124(s), 1045(s), 856(w) 780(s) and 753 cm⁻¹ assigning to O-H phenolic, CH-aliphatic, CH-iminic, C=N, C=C stretching and out of plain bending of phenolic OH and aromatic hydrogens (Fig. 5C) respectively. This work is focus on the examination of to feasibility of uptake and



Fig. 3. SEM surface properties of Porous Activated carbon before imobilization.

recovery of analytes on chemically bonded ACs for obtaining maximum signal for evaluation of these ion contents. The effective parameters *viz.* pH of sample, amount of solid phase, type and concentration of eluting agent and flow rate was optimized according to traditional one at a time optimization method.

Effect of pH on Sorption

Schiff base linkage especially when it is near the groups with potential of hydrogen bonding is relatively stable in mild acidic or basic media. Usage of Schiff base linkage for surface modification or immobilization of catalyst or enzyme (in heterogeneous enzymatic catalysis reaction) is

Fig. 4. SEM surface properties of Porous Activated carbon after imobilization.

general in many reports in the literature. A reasonable considering the sorbent structure and tracing the FT-IR spectroscopy of proposed sorbent show the presence of Schiff base linkage that as well as phenolic OH making an chelating agent (with donor atoms of N and O) on the AC surface as shown in Fig. 1 in final structure(AC-(SPIMP)). Therefore, the nature and charge of sorbent and dissociation of its surface significantly controlled by the pH. On the other hand, metal ions distribution and their complexation greatly affected by pH. The effect of pH on metal ion recoveries was examined by undertaking experiments based on constant primarily optimized value of all variables over pH range of 2-8 (Fig. 6). The highest uptake/elution yield



Fig. 5. FT-IR spectra of CNT (A), surface supported aminopropylsilylate (B), modified CNT with 2-((3-silylpropylimino)1-methyl) phenol (AC-(SPIMP))(C).



Fig 6. Effect of pH on metal ions recoveries.

was obtained at pH 5. It seems that chelate formation *via* four dentate of hydroxyl and/or nitrogen atom favorable the complication and accumulation of metal ions from solution to the sorbent surface.

The slight decrease of the uptake in the acidic media may be attributed to the protonation of the lone pair of nitrogen and oxygen that hinder the complex formation. On the other view, at low pH, due to protonation of residual AC functional groups, sorbent get positive charge and hinder from transfer of metal ions from bulk to the sorbent surface (high repulsive forces). At higher pH (pH 5), the metal ions predominantly present as M(OH)⁺ and/or insoluble precipitate of M(OH)_n. For accumulation of such substance high resistance such as dislodge of hydroxide or water molecule from metal ions atmosphere must occur and due to requirement to high energy generally is hard problem. Therefore, the low sorption/recovery of understudy metal ions occurs. This results strongly supported by considering "point of zero charge" pH (PZC). The oxidation of activated carbon with nitric acid leads to the surface fictionalizations with more oxygen-containing groups such as hydroxyl, carboxylic acid and carboxyl. The pH_{PZC} of the proposed AC-SPIMP sorbent was determined to be around 4.12 \pm 0.15. Therefore, probably at optimum pH (pH = 4), the net charge of sorbent is neutral and prominent mechanism for trapping the metal ions is their chemical reaction by sorbent loaded on AC. This fashion is more selective and repeatable. At high pH, sorption via electrostatic force (low selectivity) competes with chemical reaction.

Effect of Ratio of 2-HAP to TMSPA and Amount of (AC-(SPIMP)) on Metal Ion Recovery

The main advantage of this research is replacement of traditional non-selective functional group of AC with new Schiff base chelating agent through a chemical pathway to simultaneously increase the selectivity and usability of proposed sorbent. This chemical modification has great influence on the criterions such as hydrophobicity (sorbent and chalets) and subsequent equilibrium constant and tendency and feasibility of metal ions transfer from bulk to the sorbent surface. In this work, (AC- (SPIMP)) with high similarity to traditional Schiff base receptors seems to be an efficient material for complexation and enrichment of metal ions such as Fe³⁺ and Cu²⁺ ions.

The amount of Schiff base like chelating agent and subsequently the residual functional group of AC influenced by the ratio and amount of trimethoxysilylpropylamine (TMSPA) and 2-hydroxyacetophenone (2-HAP) (Fig. 1). The change in their ratio seems to affect the structure of



Fig. 7. Effect of amount of solid phase on metal ions recoveries.

sorbent that significantly controls the behavior of sorption systems. Preliminary experiments by conducting a set of similar experiments with chemical modification of AC show recoveries lower than 50% for all understudy metal ions. Significant enhance in the recoveries following modification show requirement of surface modification to simultaneously enhance the recoveries and probably the reusability of sorbent.

The role of ratio of sorbent material and amount of solid phase prepared at optimum ratio was investigated on the recoveries of understudy metal ions and respective results are shown in Fig. 7. It was seen that using 1 g of solid phase composed of present material (1:2 mass ratio) lead to more adsorption site and maximum recoveries was achieved. Probably at lower mass ratio due to the presence of residual functional group concern to AC or not fully chemical coupling TMSPA with HB, the sorbent surface is heterogeneous and the sorption not occur on identical sites and may their elution was occur with deficiency that lead to decrease in recoveries (Table 2 and Fig.7). Results of Fig. 6 show that by increase in the solid phase amount till 1 g a significant enhances in recoveries was achieved. At higher amount of solid phase probably eluting solution is insufficient for efficient elution of this metal ion. With a lower amount, the extent of complexation and retention of metal ions on the loaded solid phase is low and hence the recovery was decreased.

Effect of Eluents Type and Volume

Various selection of eluent is possible by combination of

approaches such as using organic solvent, acidic solution or their simultaneous application to desorbs retained analytes [42-45]. Among them using acidic solution lead to efficient and repeatable elution of retained metal ions without destruction of solid phase that was used in this research. Desorption of retained metal ions was carried out in the presence of various concentration, type and volume of eluent recommended by Table 3. Presented results clearly show that using 6 ml of 4.0 M of nitric acid is best eluent for elution of possible high analytes to make preconcentration factor and their simultaneous determination.

Finally, 6 ml of 4 M HNO_3 was taken as the eluent for desorption of metal chelates from (AC- (SPIMP)) and was used for the optimization of the other parameters.

Flow Rates of Sample and Eluent Solutions

The sample and eluent flow rate not only control the analysis time, but also significantly affect the analyte deposition on the sorbent surface. The sample loading rate has distinguished role in retardation of metal ions *via* sorbent while the flow of eluent solutions affects their recoveries and subsequently duration of complete analysis. Therefore, the effect of flow rate was examined under the optimum conditions (pH, eluent, amount of support and modifier, *etc.*) using 250 ml of sample solution. For both variables, the flow rate was adjusted in the range of 1.0-4.0 ml min⁻¹. It was found that the analytes loading due to chelation was practically not changed up to 2 ml min⁻¹ flow

Ratio of 2-HAP to TMSPA	Recovery (%)		
	Cu	Fe	
1.6/2.6	62	65	
1.4/2.4	60	57	
1.1/2.2	64	69	
1.0/2.0	81	84	
0.9/1.8	98	98	
0.7/1.4	63	61	

 Table 2. Effect of Ratio of 2-HBA to TMSPA on Metal Ion Recovery

Table 3.	Effect	of	Туре	and	Concentration	of	Eluting
	Agen	t on	Reco	very	of Analytes		

Condition of almost	Recovery (%)			
	Cu	Fe		
6 ml of HCl (4.0 M)	75 ± 2	79 ± 1		
6 ml of H ₂ SO ₄ (4.0 M)	49 ± 3	65 ± 2		
6 ml of CH ₃ COOH (4.0 M)	39 ± 3	45 ± 2		
6 ml of H ₃ PO ₄ (4.0 M)	56 ± 3	35 ± 3		
6 ml of HNO ₃ (2.0 M)	64 ± 2	82 ± 3		
6 ml of HNO ₃ (4.0 M)	98 ± 1	98 ± 1		
6 ml of HNO ₃ (5.0 M)	77 ± 2	90 ± 1		
6 ml of HNO ₃ (6.0 M)	96 ± 1	93 ± 3		
2 ml of HNO ₃ (4.0 M)	61 ± 1	57 ± 2		
4 ml of HNO ₃ (4.0 M)	80 ± 3	83 ± 2		
8 ml of HNO ₃ (4.0 M)	96 ± 1	98 ± 1		

rate, and the recoveries of decreased significant when the flow rates over 1 ml min⁻¹. Thus, these values were selected in further steps to optimize other variables.

Sample Volume and Enrichment Factor

To obtain reliable and reproducible analytical results and high concentration factor, it is very important to get satisfactory recoveries for retained analytes from large volume sample solutions as [46-52]. The effect of sample volume on the loading of the metal ions by dissolving a fixed value of analytes (50 μ g) in diverse volume (250-1500 ml) was examined and it was seen that the metal ions, quantitatively was sorped-desorped until 750 ml that known as break through volume. At higher volume probably due to possible saturation of sorbent surface or repulsive force between the adsorbed metal ions and respective ions in bulk solution a significant decrease in the removal percentage was observed. The preconcentration factor for simultaneous loading of analytes (the ratio of the maximum sample volume for analyte (750 ml) to the lowest final eluent volume (6.0 ml)) was observed to be 125. The adsorption capacity shows the applicability of sorbent for metal ions removal from large sample volume and/or high saline content. The sorption capacity was calculated based on Langmuir model as acceptable model based on the homogenous adsorption as monolayer without interaction expressed in the following linear form [53]:

$$C_e/q_e = 1/k_L q_m + C_e/q_m \tag{2}$$

where q_{max} represents the maximum sorption capacity and obtained from slope of achieved line by plotting C_e/q_e against C_e over series of concentrations (50-300 µg ml⁻¹) at appropriate pH. The q_{max} is 45.3 mg g⁻¹ that is very higher than commercial AC value (1.46 mg g⁻¹).

Effect of Interfering Ions

As it is known, due to presence of strong wavelength selector and high selectivity hallow cathode lamp and correction of background, FAAS based determination has high selectivity and accuracy. The expected interference may be attributed to concomitant anions and/or cations through their possible binding with chelating agents and/or metal ions. The possible interference of other metal ions and few anions on the recoveries of Cu²⁺ and Fe³⁺ ions was investigated by conduction similar SPE experiments in the presence and absence of interference and the results are summarized in Table 4. The judgment about the possible interference considered was relative error of less than 5%. Concentration leads to such deviation level in preconcentration and/or determination stage (up to 5%) known as tolerance limit. It could be seen that some ions at 1000 fold mass ratio has not significant influence on interference-free analytes recoveries. Thus, the determination level of present system indicates that high

Ion	Added As	Tolerance Limit
		$(mg l^{-1})$
Na ⁺	NaCl	1000
\mathbf{K}^+	KCl	
Cl	NaCl	
CH ₃ COO ⁻	CH ₃ COO Na	650
Mg^{2+}	$MgCl_2$	600
HCO ₃	NaHCO ₃	800
Sr ²⁺ , Cd ²⁺ , Ba ²⁺ , Ca ²⁺ , Mn ²⁺	Nitrate salt	250
Zn^{2+} , Ni^{2+} , Co^{2+} , Pb^{2+} , Ag^+ , Al^{3+} , Hg^{2+}		

Table 4. Effects of the Matrix Ions on the Recoveries of the Examined Metal Ions (N = 3)

Table 5. Specification of Presented Method at Optimum Conditions for each Element

Parameters	Cu	Fe
Linear range (µg ml ⁻¹)	0.01-0.28	0.02-0.24
Correlation coefficient (R^2)	0.995	0.986
Detection limit (ng ml ⁻¹)	1.2	2.6
RSD (repeatability) (%)	3.0	3.2
Recovery (repeatability) (%)	96.9	97.0
RSD (reproducibility) (%)	2.8	2.7
Recovery (reproducibility) (%)	98.5	98.2
Loading capacity (mg g ⁻¹)	41.4	45.3
Enrichment factor	28.0	21.5

concentration of matrices constituent permit very low minimal influence on the sorption-recoveries and determination of analytes.

Analytical Features

One of most important properties of each method is applicability for trace metal ions determination which is limit by its detection limit. At optimum values of all variables, the method was subjected to various concentrations of analytes and also blank solutions. According the traditional definition of IUPAC, the characteristics performances of the method are presented in Table 5. The limit of detection (LOD) and empirical limit of quantification (LOQ) based on the three and ten times of the

ions in complicated matrices was tested by its subjection with real samples including banana, pineapple, tomato and radish. The accuracy and repeatability was tested by three

Accuracy and Applications

replicate using standard addition method and respective results is shown in Tables 6 and 7. The recoveries more than 95% and RSD lower than 3.5% show the capability of the novel method for simple and easy, low cost determination

standard deviation of the blank (n = 10) was found to be

1.3-2.6 and 8-15 μ g ml⁻¹. The method benefit from

advantages such as wide linear range, low detection limit, high recoveries (>94%) and acceptable RSD% (<3.5%).

The usage of proposed method for evaluation of target

Ion	Added ($\mu g g^{-1}$)	Found ($\mu g g^{-1}$)	RSD (%)	Recovery (%)
		Tomato		
Fe	0	9.81	3.9	-
	10	19.25	3.3	94.4
Cu	0	7.06	4.1	-
	10	17.25	3.5	101.9
		Radish		
Fe	0.0	12.3	3.8	-
	10	22.6	3.2	103.0
Cu	0.0	8.9	4.2	-
	10	18.7	2.9	98.0

Table 6. Recovery of Analytes from Spiked Samples by Using Proposed Method (N = 3)

Table 7. Levels of Analyte Ions in Real Samples (N = 3)

Pinea	pple			Banana			
Ion	Added	Found	RSD (%)	Recovery (%)	Found	RSD	Recovery
	value	value					
E.	0	33.4	3.8	-	25.3	3.8	-
ге	10	43.7	3.2	104.0	35.7	3.3	104.0
Cu	0	19.6	3.7	-	21.82	3.9	-
Cu	10	29.3	3.3	97.0	32.09	3.3	102.7

The value are for solid samples is $\mu g g^{-1}$.

of analytes. The recovery of spiked samples is satisfactory reasonable and was confirmed using standard addition method

CONCLUSIONS

This work focuses on the synthesis and characterizations of novel low cost sorbent. The sorbent was characterized using SEM, BET and FT-IR as powerful identification techniques. Due to presence of high surface area (1317.1346 m² g⁻¹) and nanometer scale and pore size (average pore size of <37.750 A) and scale around 80 nm, has high ability to enrich metal ions *via* various pathway such as chemical binding with Schiff base like chelating agent and trapping into the interior core of sorbent.

The method was simple, easy and also rapidly applied for environmental samples including fruit samples with high enrichment factor (21.5-28) and low LOD (in the range of 1.2-2.6 ng ml⁻¹) and acceptable RSD (<4.5%) in real samples.

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